



Dynamic Behaviour and Operational Flexibility of the ATP Processor

International Oil Shale Symposium, Tallinn 2013

Steven Odut, P.Eng.



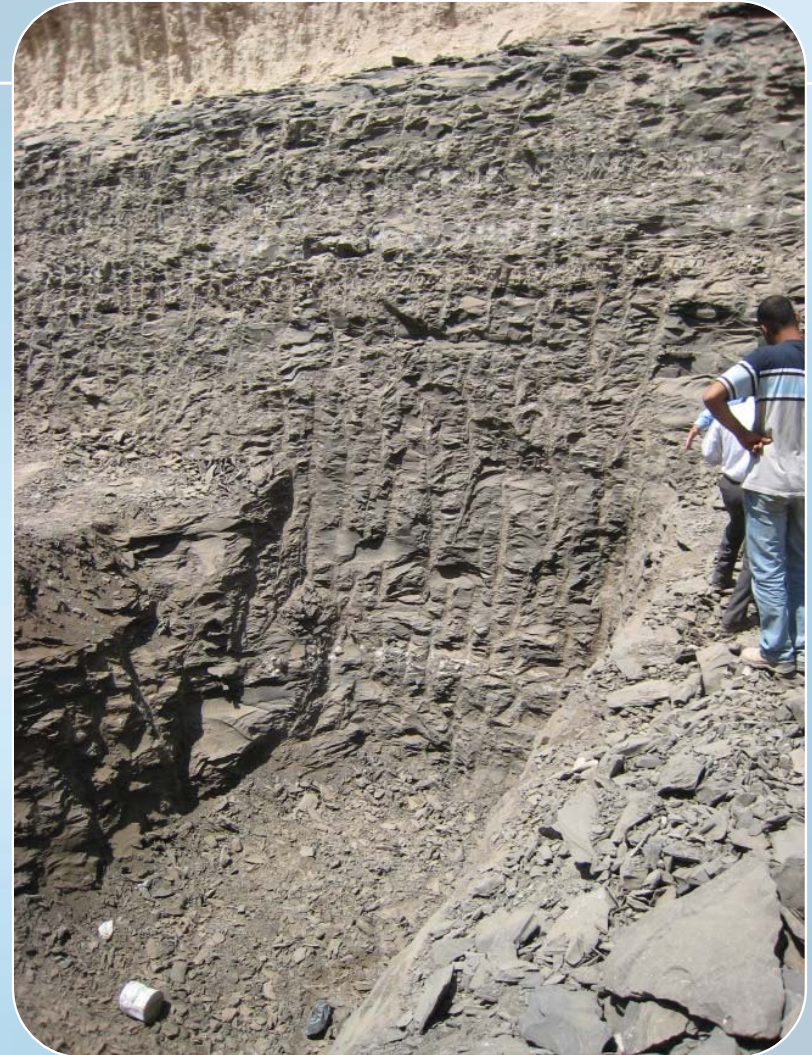
Mineable Oil

Shale oil^(*) is mineable oil.

* Not that stuff they pump out of the ground

A good miner will deliver consistent feed to the process plant – but there will be variability.

The process plant must accommodate ore variability and provide sufficient flexibility to respond to operational challenges.



Shale oil production starts at the mine

Case Studies

Kerosene Creek Oil Shale

Free moisture	Design 24%	Actual 20-27%
After dryer	Design 8%	Actual 8 to 18%
Kerogen	Design 27%	
Horizons	A, B1, C1 a.b.c.d.e , C2, D1, D2 , E	
Other surprises	Siderite nodules	
	Thermal sensitivity during drying	
	Emission and oil quality impacts	
Tropical rainstorms (+100 mm per hour)		

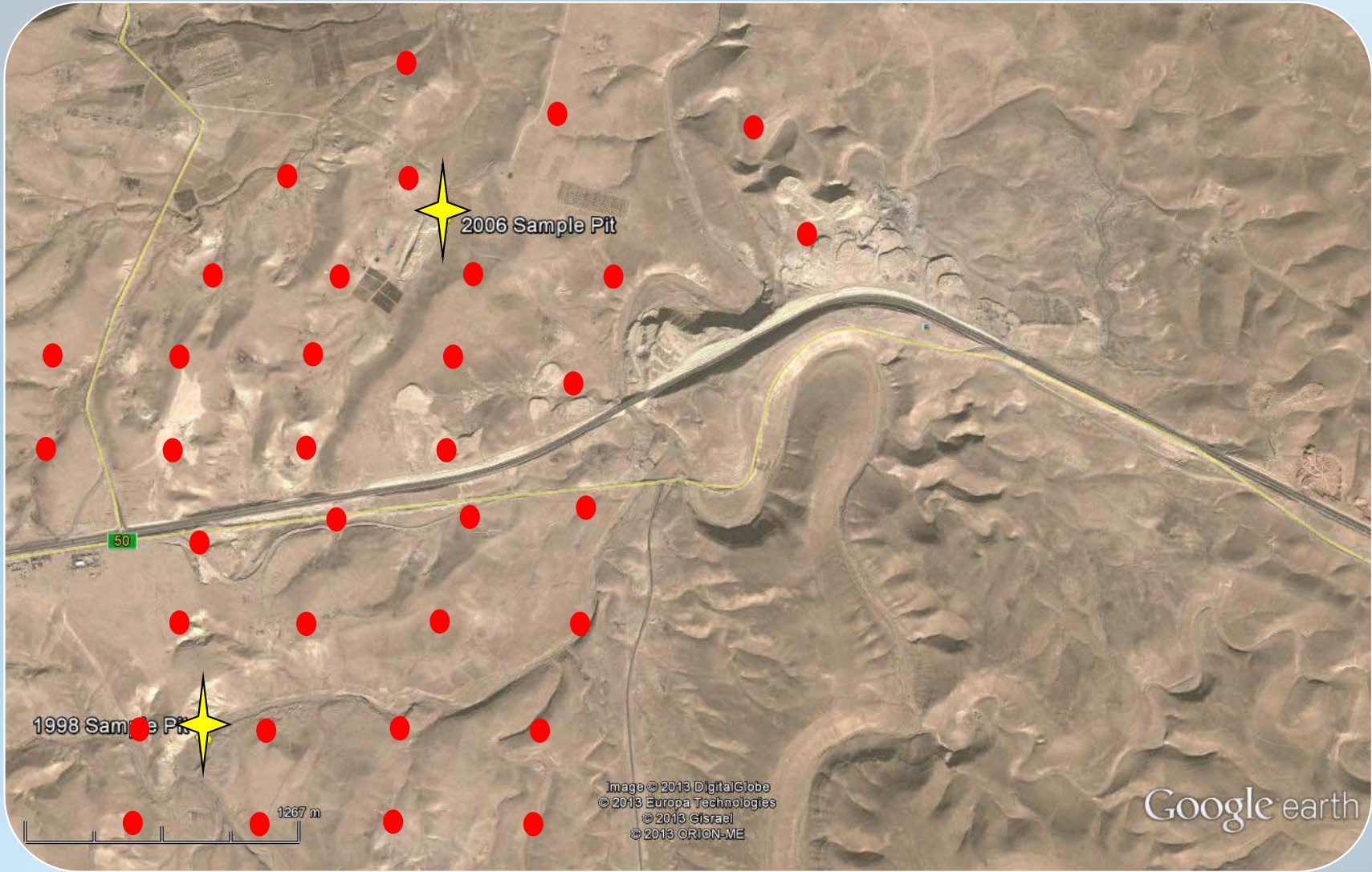


Al Lajjun Oil Shale

Free moisture	Design 3%	Actual 3-6% (100% variation)
Kerogen	Design 22%	Actual 15-26% and soluble bitumen present
Horizons	A0, A1, B, C, D , M	

The miners must deliver what the plant wants.
The plant must accept what the miners deliver.

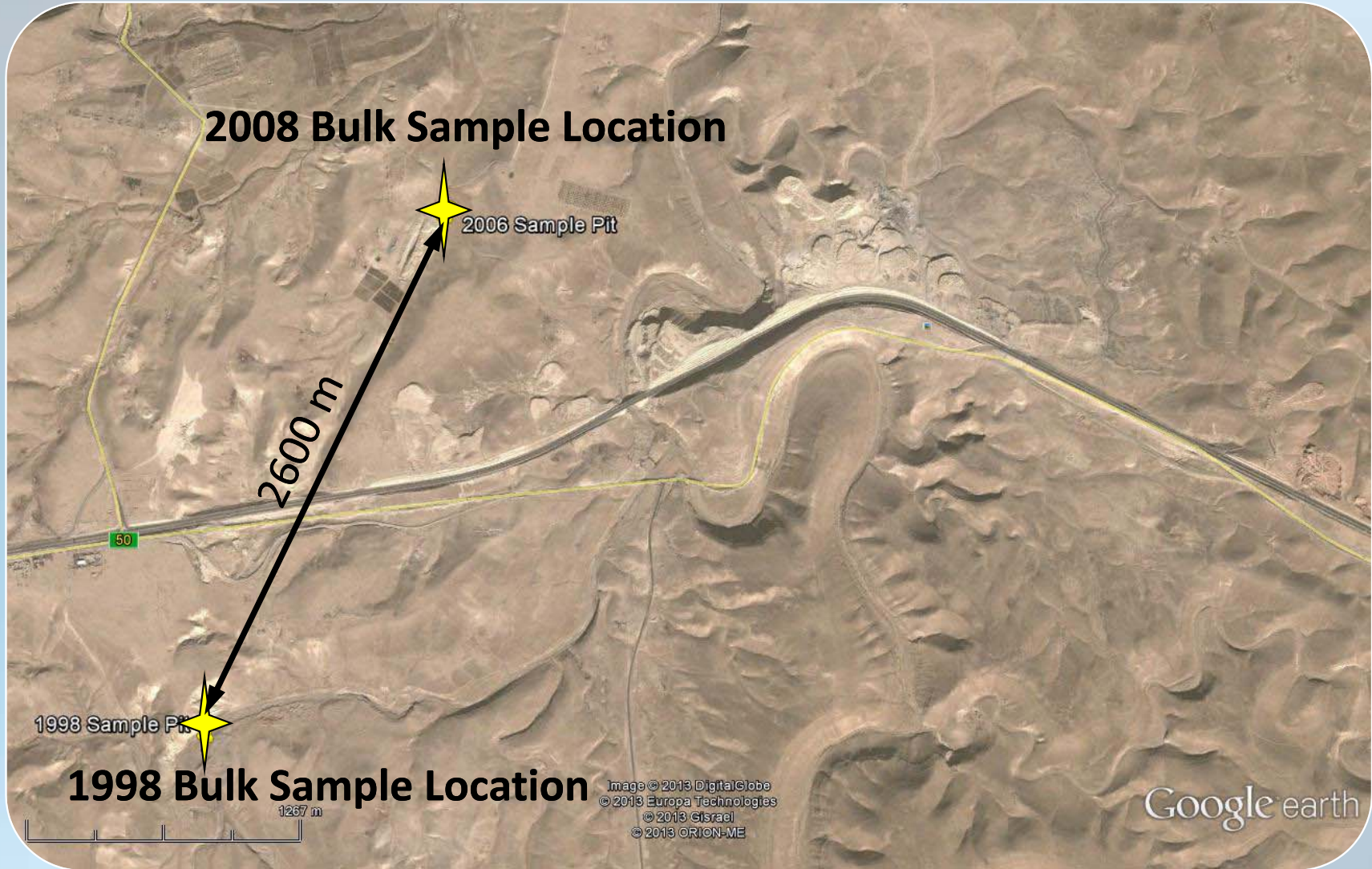
Geological Variation



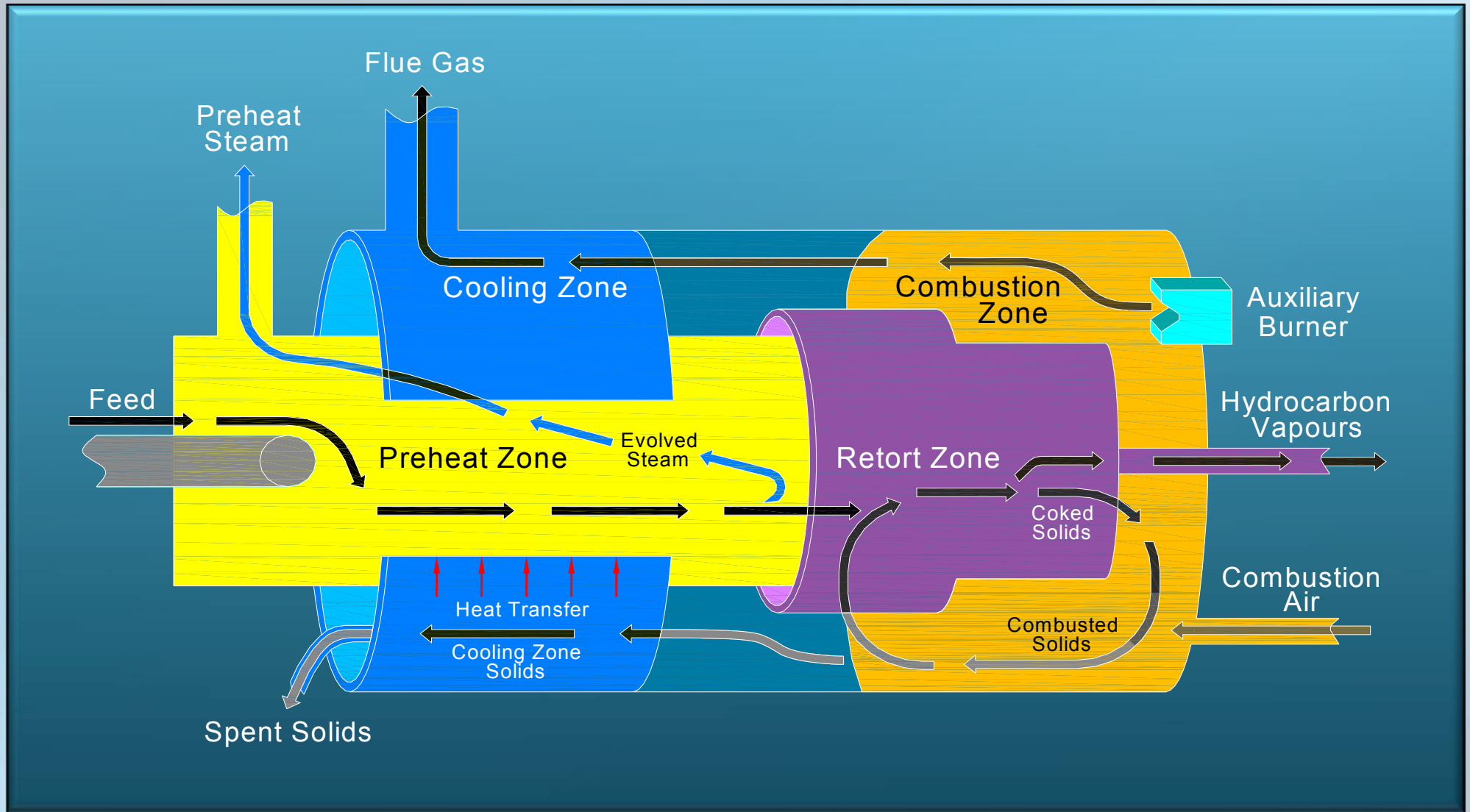
Geological Variation



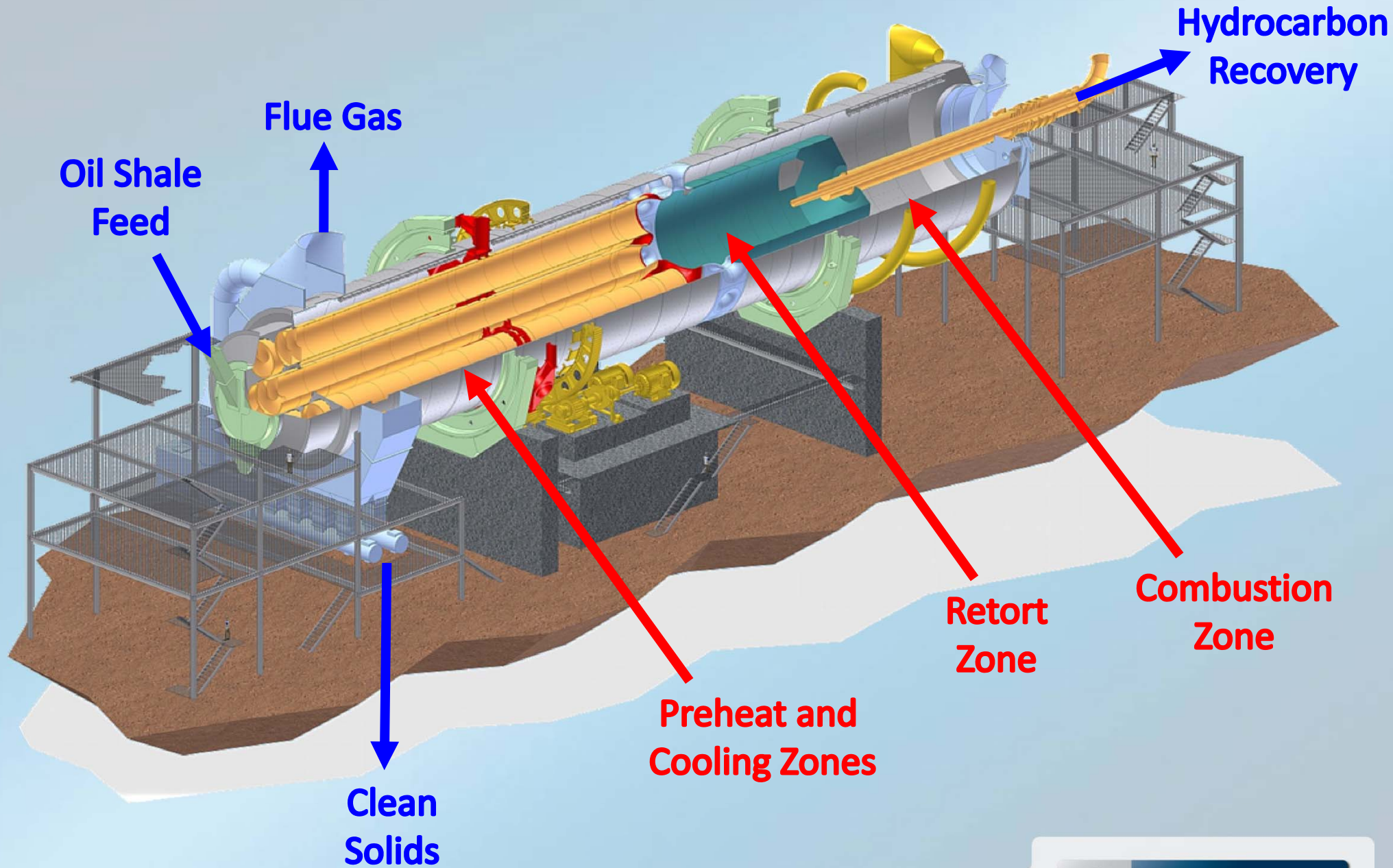
Geological Variation



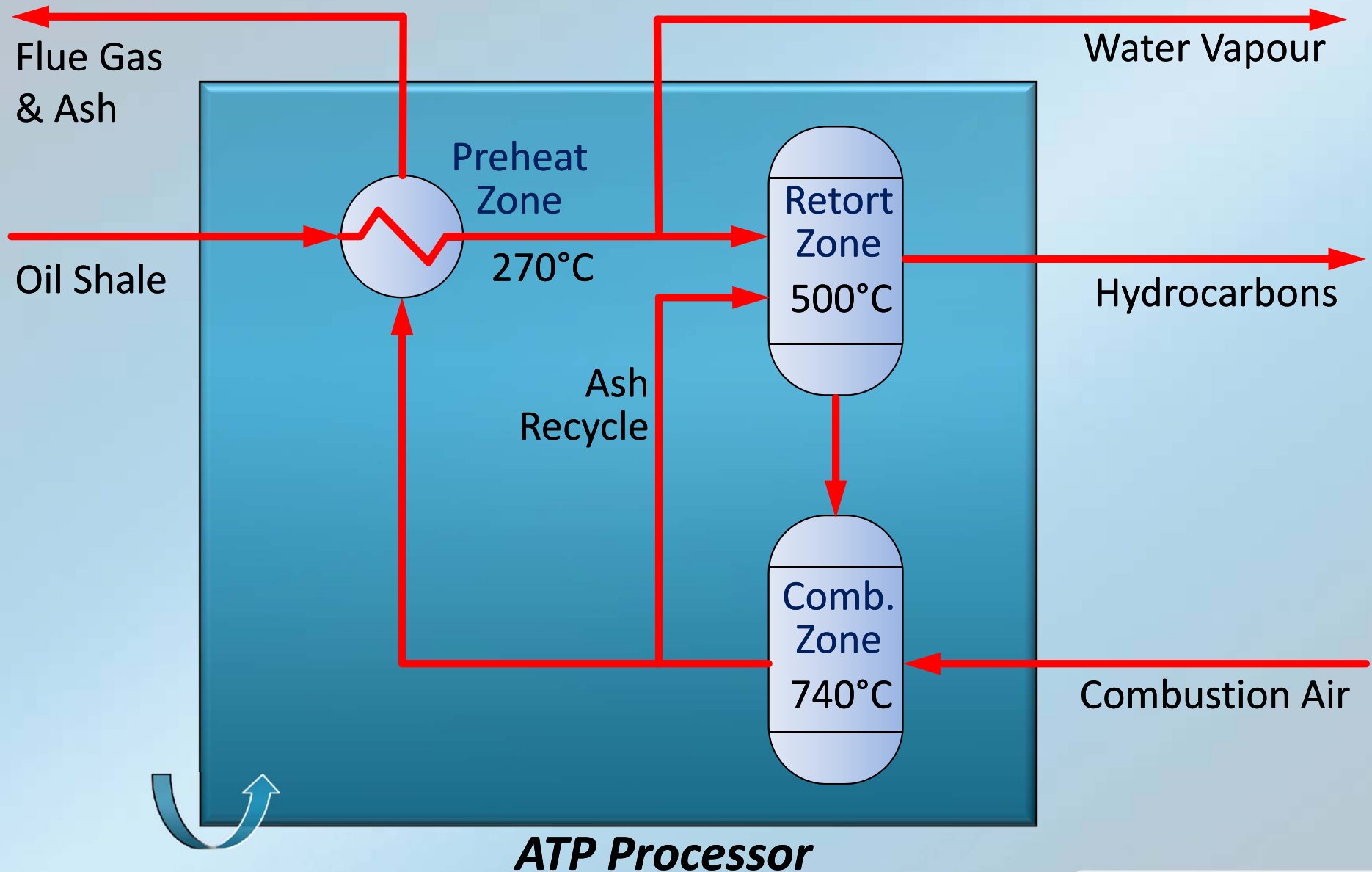
The ATP Processor



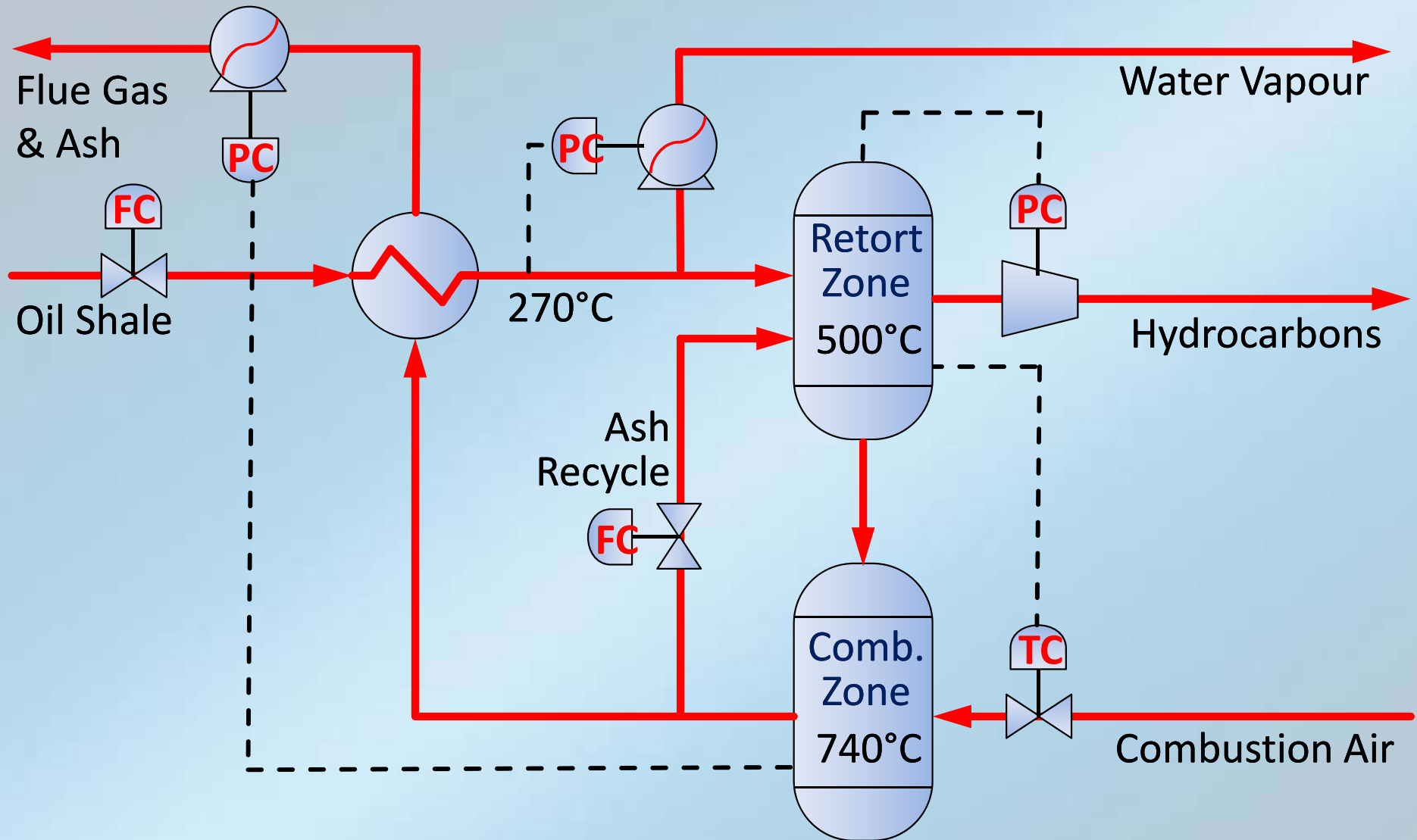
The ATP Processor Mechanical Arrangement



The ATP Processor Depicted as Discrete Process Vessels



The ATP Processor – Process Control

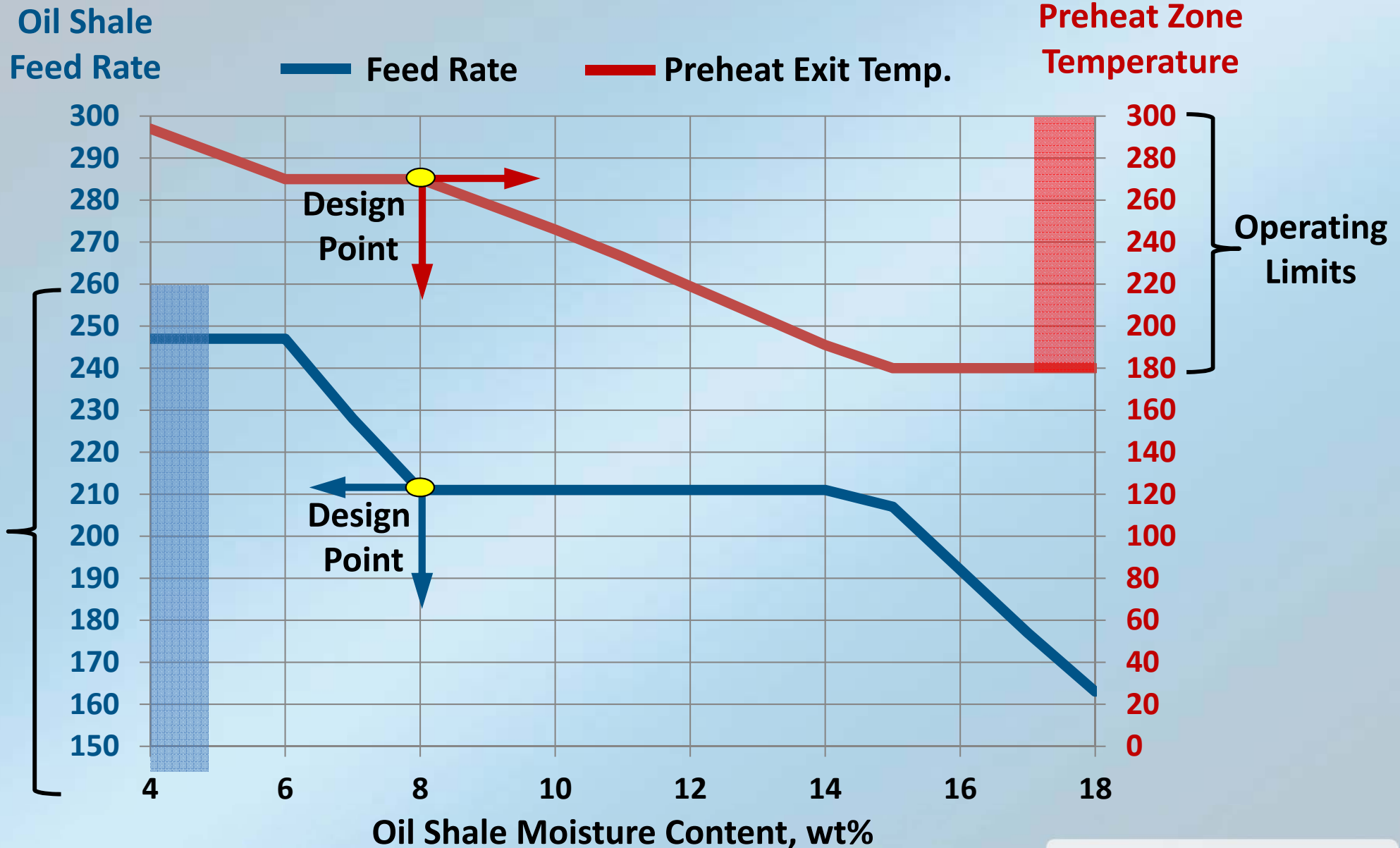


The ATP Processor - Process Control Boundaries

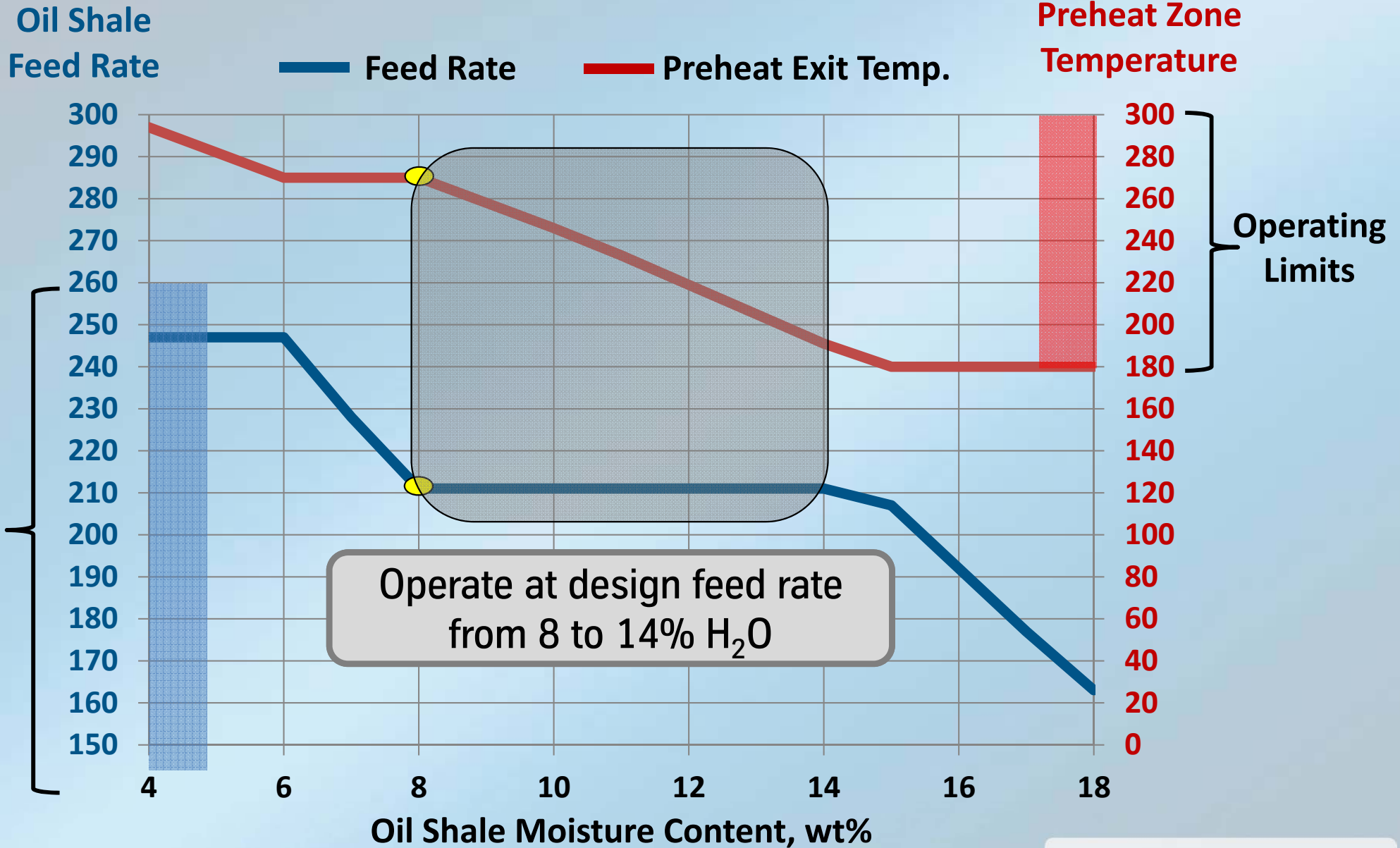
	Oil Shale Feed Rate, t/h	Preheat Temp, °C	Retort Temp, °C	Combustion Temp, °C
Low Limit	100	180	475	675
Normal Target	211	270	505	740
High Limit	265	300	550	760
Low Limit Reason	HC system turndown	Shale not dry before retort	Reaction kinetics	Combustion kinetics
High Limit Reason	Flow of solids through ATP	Premature pyrolysis	Excessive pyrolysis	Metallurgy

Retort temperature controlled +/- 5°C of target
 Preheat & combustion temp. fluctuate within acceptable bounds
 Oil shale rate maximized until system bottleneck approached

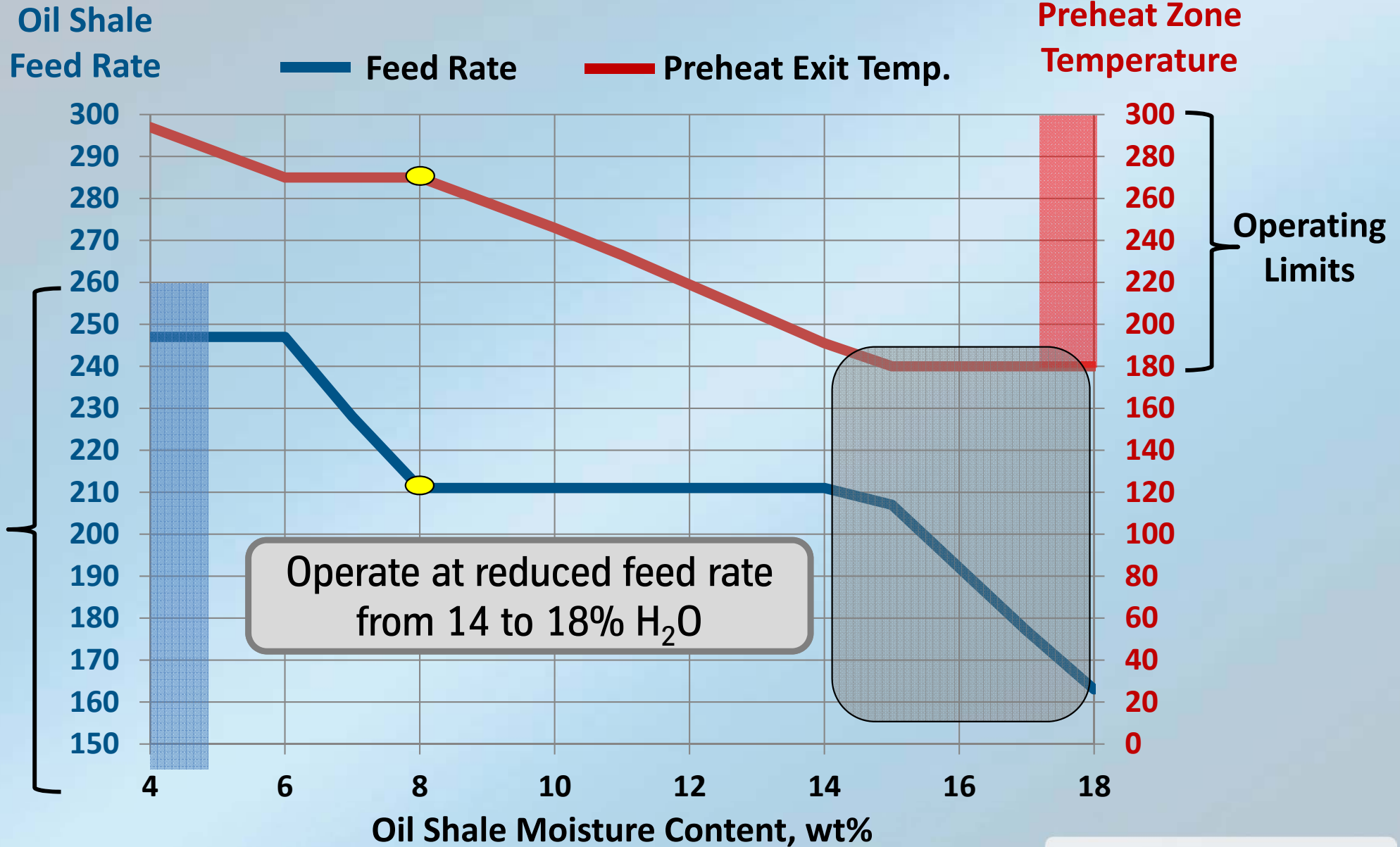
Example: Feed Moisture – Operation from 4 to 18% H₂O



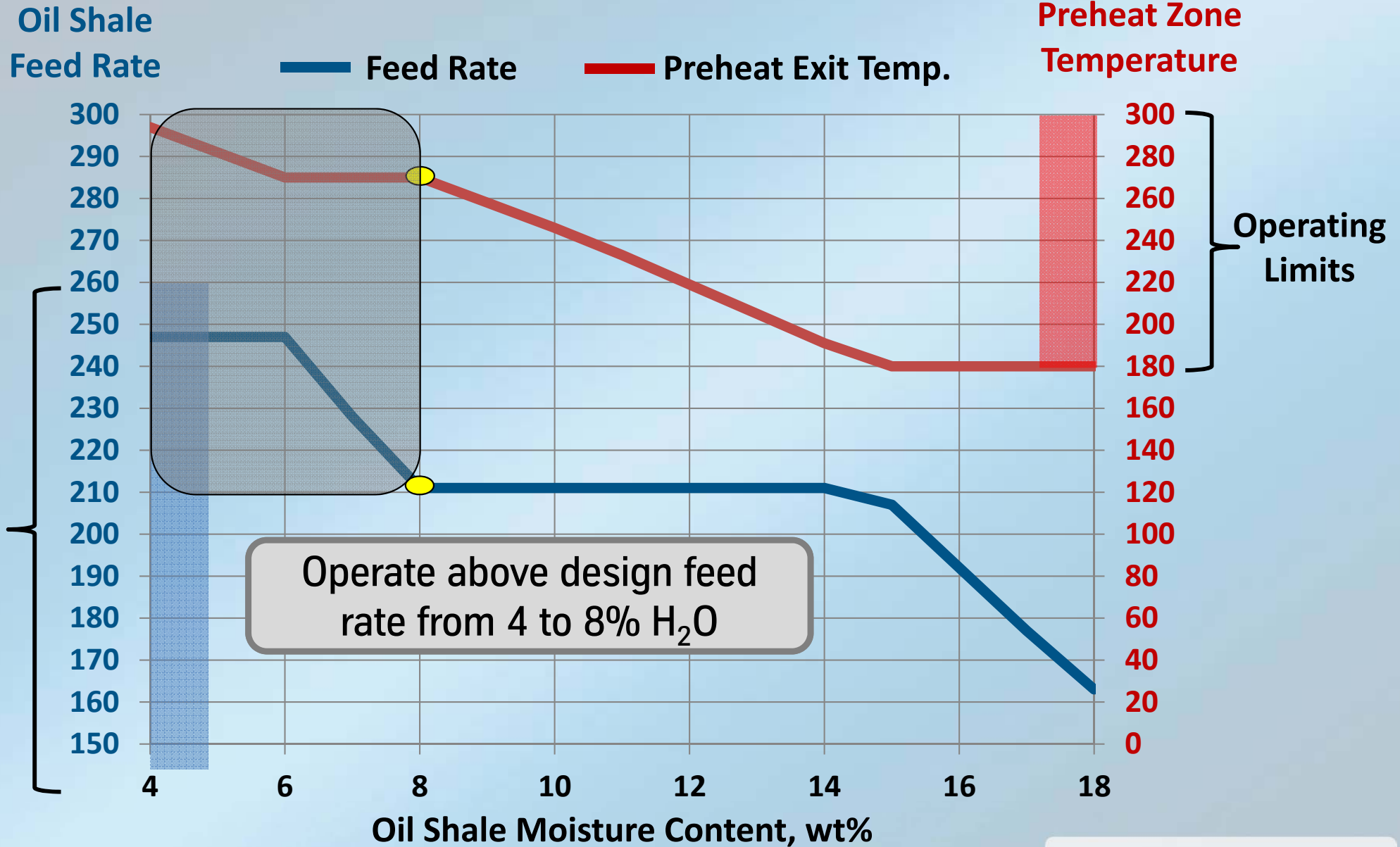
Example: Feed Moisture Content



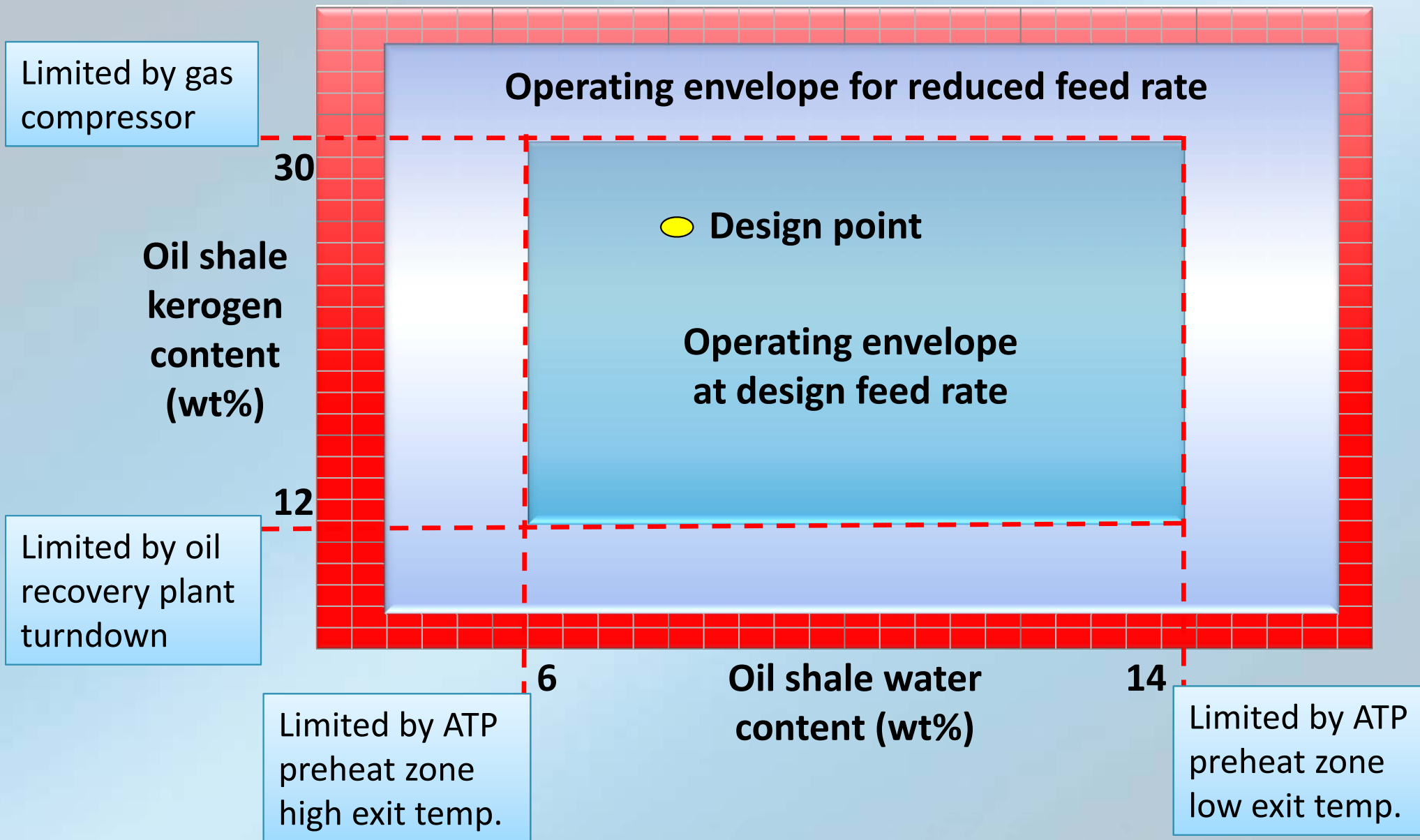
Example: Feed Moisture Content



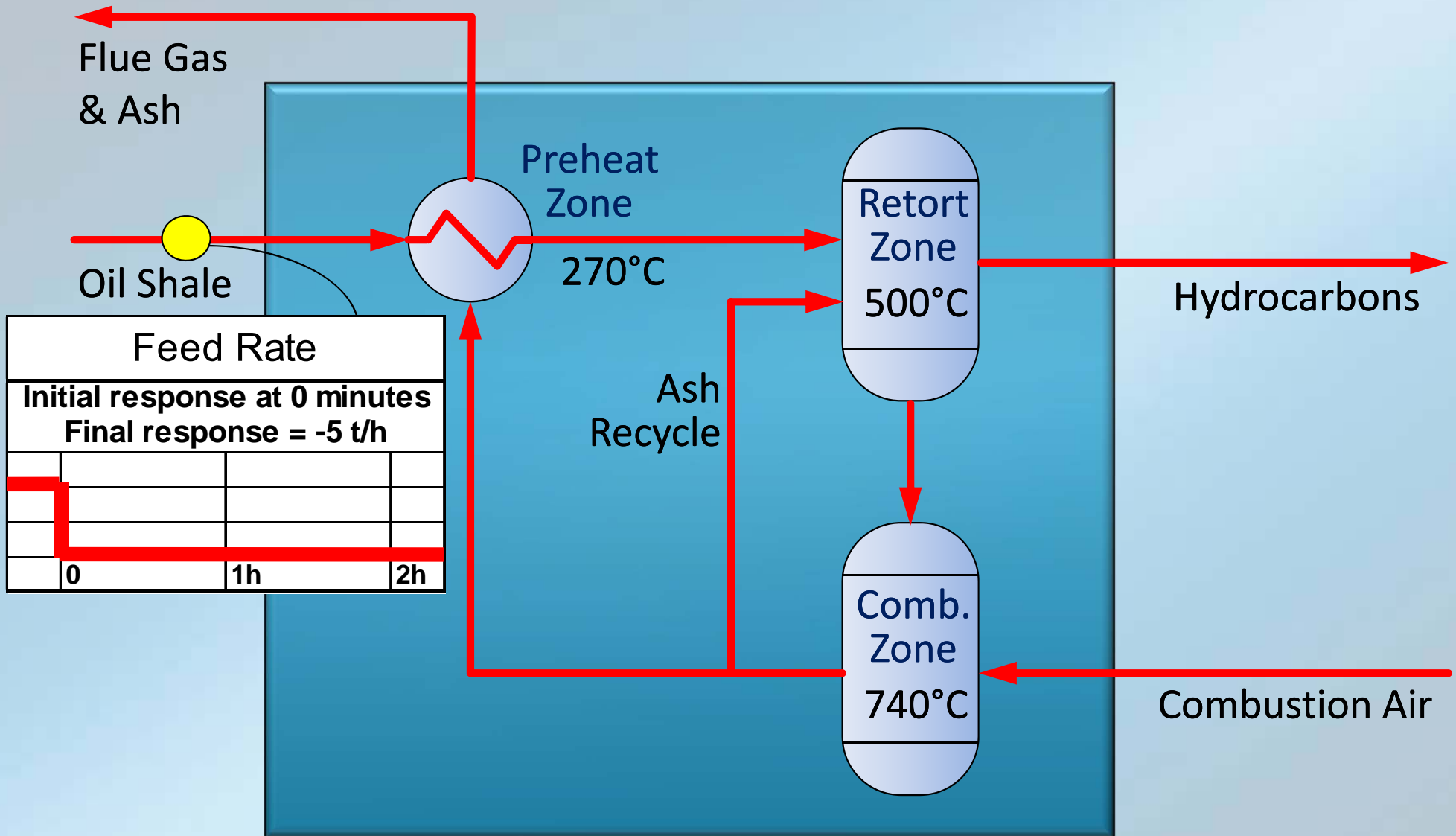
Example: Feed Moisture Content



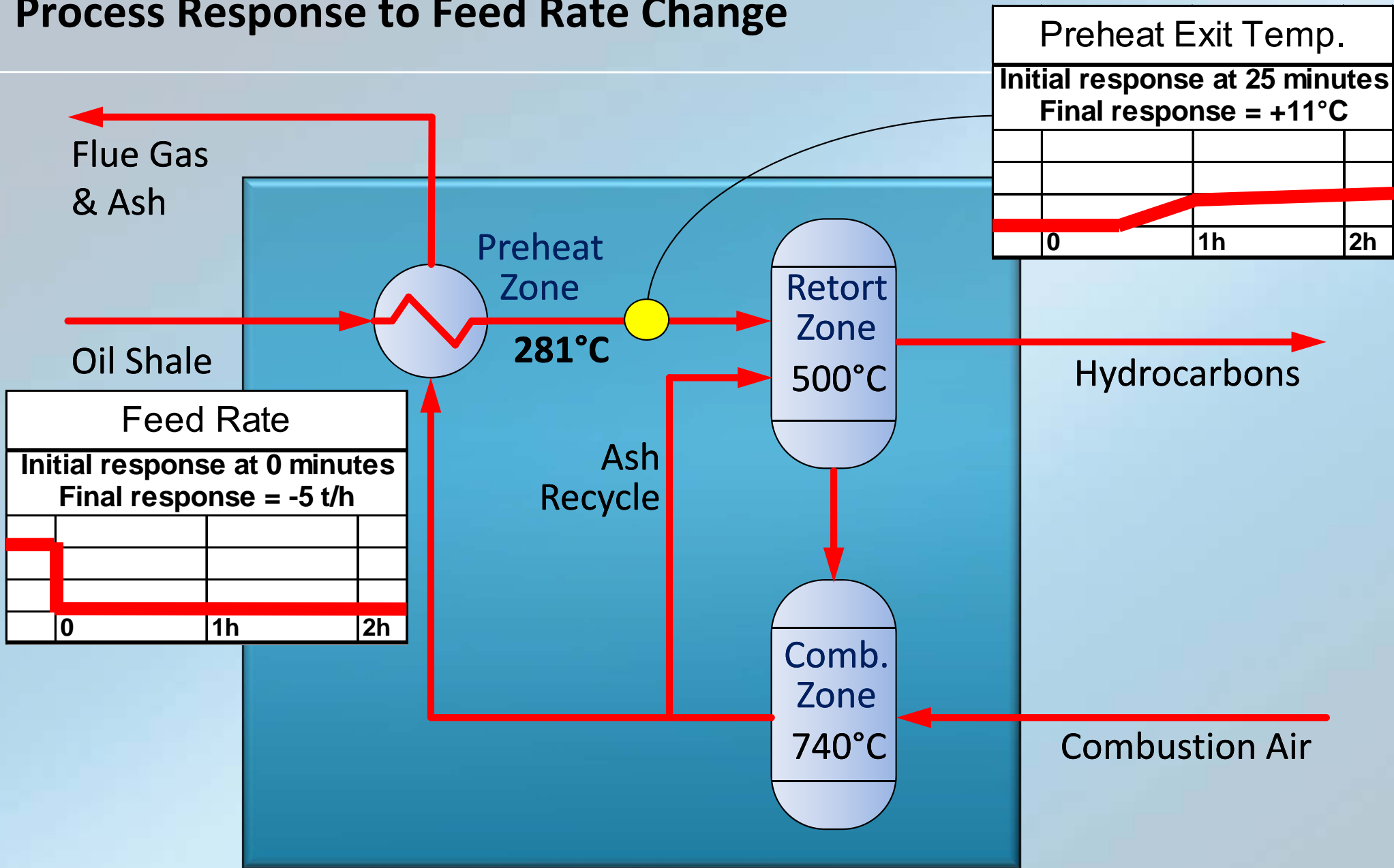
The ATP Processor - Wide Operating Envelope



Process Response to Feed Rate Change



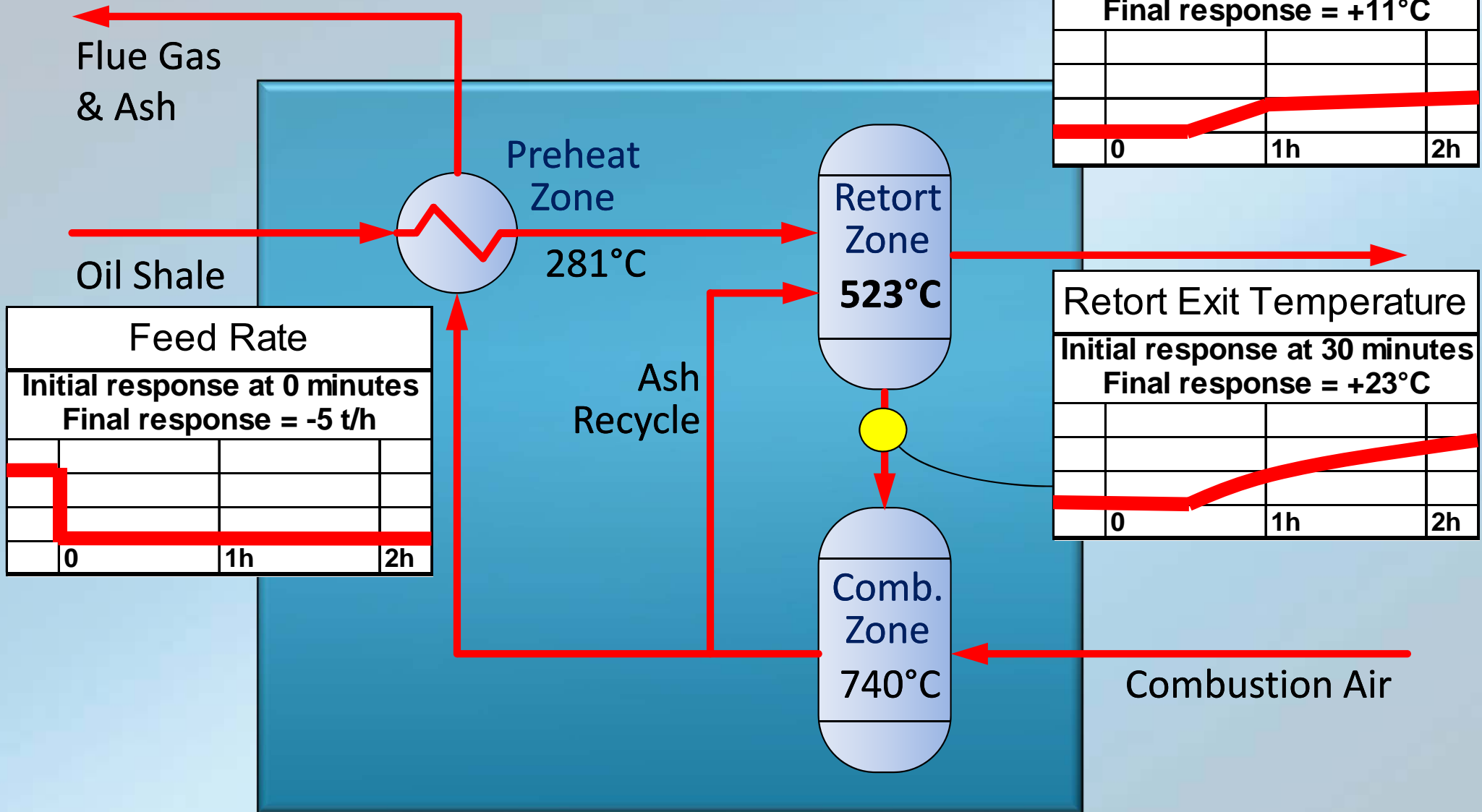
Process Response to Feed Rate Change



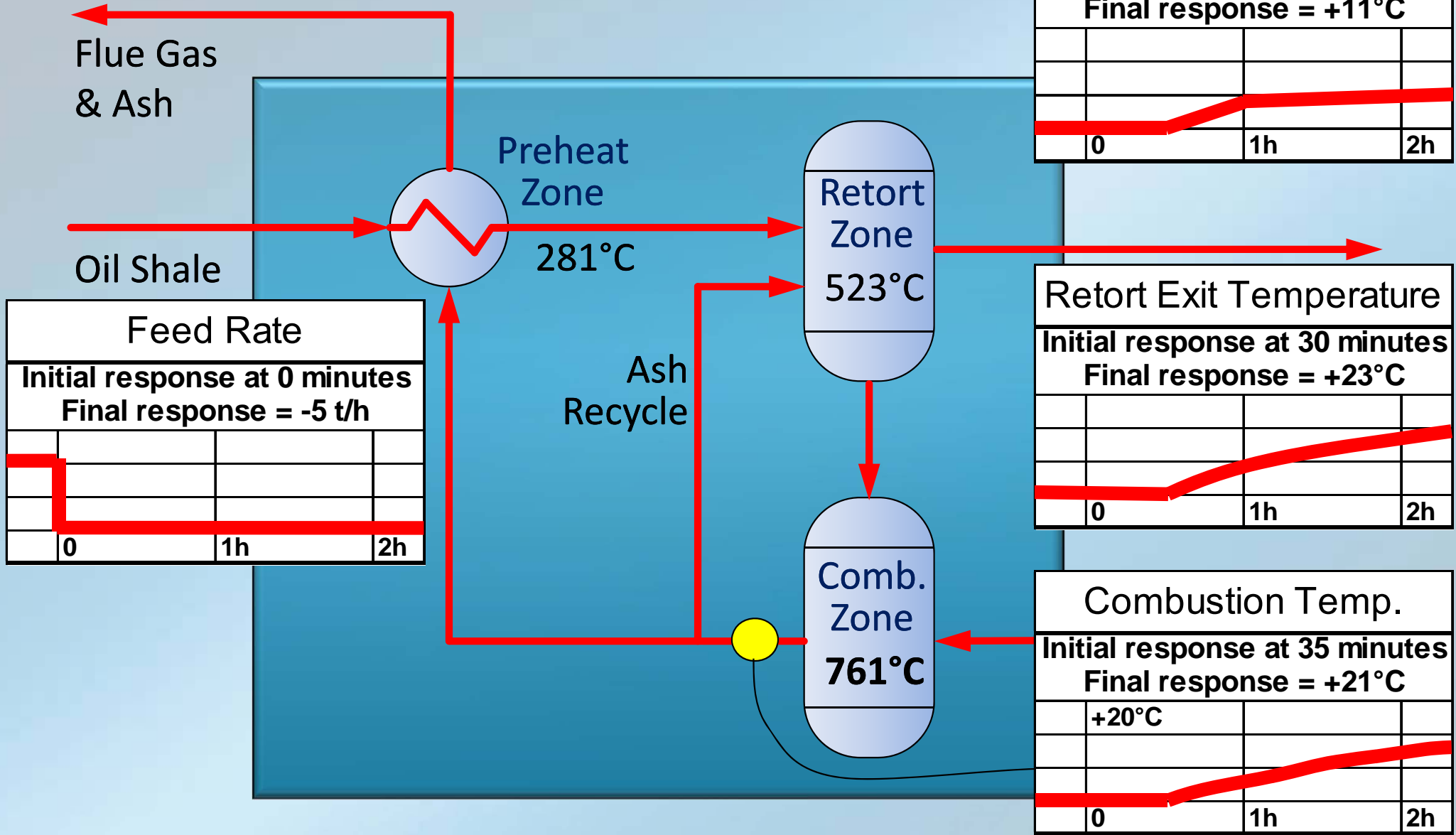
Feed Rate			
Initial response at 0 minutes			
Final response = -5 t/h			
0	1h	2h	

Preheat Exit Temp.			
Initial response at 25 minutes			
Final response = +11°C			
0	1h	2h	

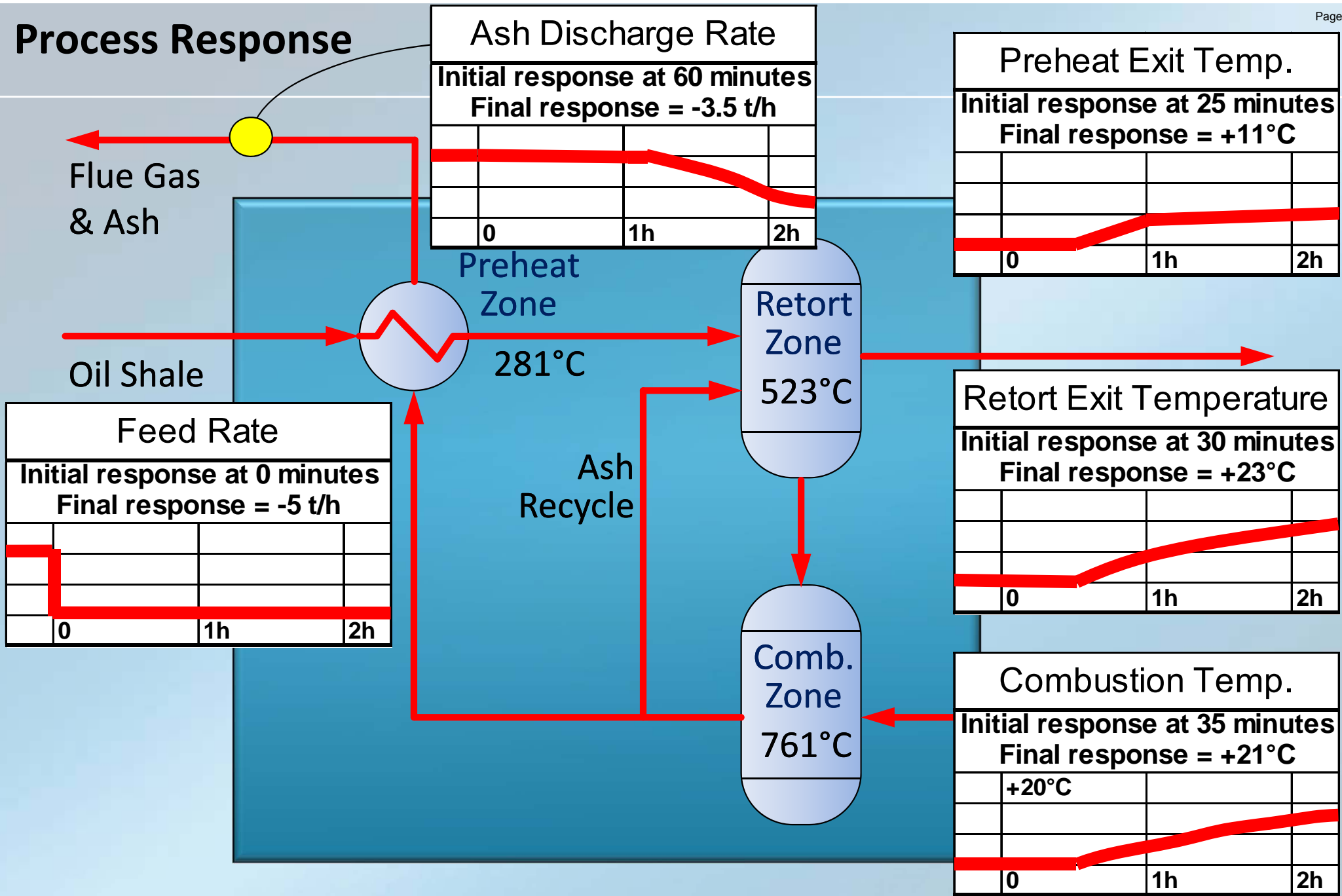
Process Response to Feed Rate Change



Process Response to Feed Rate Change



Process Response



Stable and Predictable Responses

Input Variable	Input Change	Preheat Exit Temperature	Retort Exit Temperature	Combustion Temperature	Ash Discharge Rate
ATP Oil Shale Feed Rate	5 t/h ↓	Initial response at 25 minutes	Initial response at 30 minutes	Initial response at 35 minutes	Initial response at 60 minutes
		Final response = +11°C	Final response = +23°C	Final response = +21°C	Final response = -3.5 t/h
		+20°C	+20°C	+20°C	0
		0	0	0	-4 t/h
Coke Combustion Air Rate	2.5% ↑	Initial response at 10 minutes	Initial response at 15 minutes	Initial response at 1 minute	Initial response at 1 minute
		Final response = +14°C	Final response = +28°C	Final response = +34°C	Final response = 0 t/h
		+20°C	+20°C	+20°C	+4 t/h
		0	0	0	0
Recycle Gate Position	40 t/h ↑	Initial response at 10 minutes	Initial response at 2 minutes	Initial response at 10 minutes	Initial response at 10 minutes
		Final response = -2°C	Final response = +10°C	Final response = -6°C	Final response = 0 t/h
		+10°C	+10°C	+10°C	0
		0	0	0	-10 t/h
ATP Rotational Speed	0.3 rpm ↑	Initial response at 5 minutes	Initial response at 5 minutes	Initial response at 5 minutes	Initial response at 5 minutes
		Final response = +1°C	Final response = +3°C	Final response = +3°C	Final response = 0 t/h
		0	0	0	+10 t/h
		-20°C	-20°C	-20°C	0



Concluding Remarks



Ore Feed Flexibility

- Ore variability will occur.
- ATP Systems are designed for specific oil shale, but are fully capable of handling a range of grade and moisture contents, giving operators increased flexibility in mine planning and plant operation.



Operational Stability

- ATP Processor is large rotary mineral processing unit which provides stable material handling and thermal processing.
- Predictable and controllable.
- Rotary machines are recognized for their tolerance to variations in feed and to transient operations.



Decoupling

- Important to decouple process units so that upsets do not propagate through multiple systems.

Questions?



谢谢 Thank You شكرا
Kiitos Vielen Dank Merci
Aitäh Спасибо

Definitions / Legend

ATP	Alberta Taciuk Process
bbbl	Barrel of Oil (~159 Litres)
°C	Degrees Celsius
FC	Flow Control
HC	Hydrocarbons
LTOM	Litres of Oil Per Tonne Of Zero Moisture Ore
PC	Pressure Control
rpm	Rotations per Minute
SCO	Synthetic Crude Oil
t/h	Metric Tonnes per Hour
TC	Temperature Control
Temp.	Temperature
wt%	Weight Percent



Contact Information

UMATAC Industrial Processes Inc.
Suite #110, 6835 Railway Street S.E.
Calgary, Alberta, Canada
T2H 2V6

Telephone: +1-403-910-1000

Facsimile: +1-403-910-1040

email: umatac@thyssenkrupp.com

web: www.umatac.ca

